

ERRATA

N. S. Grewal and S. C. Saxena, Heat transfer between a horizontal tube and a gas-solid fluidized bed, *Int. J. Heat Mass Transfer* **23**, 1505-1519 (1980).

Table 1: Ainshtein [14] correlation should read:

$$Nu_{wT} = 5.76(1-\epsilon)(G\bar{d}_p/\mu\epsilon)^{0.34} Pr^{0.33} (H_d/D_b)^{0.16} (D_T/\bar{d}_p)$$

where H_d is the height of heat transfer tube above the distributor plate.

Table 1: The correlation of Genetti *et al.* [17] should read:

$$Nu_{wT} = \frac{11(1-\epsilon)^{0.5}}{\left[1 + \frac{0.2512}{(G\bar{d}_p/\mu)^{0.24} (\bar{d}_p/0.000203)^{1.23}}\right]^2} (D_T/\bar{d}_p).$$

In Fig. 8: the vertical axis should read:

$$Nu_{wT}/[(1-\epsilon)Pr^{0.33} (H_d/D_b)^{0.16} (D_T/\bar{d}_p)].$$

In Fig. 12: the horizontal axis should read:

$$\log \left[1 + \frac{0.2512}{(G\bar{d}_p/\mu)^{0.24} (\bar{d}_p/0.000203)^{1.23}}\right]^2.$$

P. Hrycak, Heat transfer from a row of impinging jets to concave cylindrical surfaces, *Int. J. Heat Mass Transfer* **24**, 407-419 (1981).

In the caption to Fig. 10, change the expression for Nu_0^* to $Nu_0^* = Nu_0 Pr^{-0.39} (D_c/D)^{0.42} (Z_n/D)^{0.22} (C_n/D)^{0.16}$.

In the caption to Fig. 12, change the expression for Nu^* to $Nu^* = Nu (D_p/D)^{0.402} (D_n/D)^{0.16}$.

Also, in this caption, change "sith" to "with".

In Reference 37, change "Ludwig" to "Ludwig".

J. S. Vrentas, R. Narayanan and S. S. Agrawal, Free surface convection in a bounded cylindrical geometry, *Int. J. Heat Mass Transfer* **24**, 1513-1529 (1981).

All entries in Table 9 on p. 1525 should be labelled "DOWN" rather than "UP".

The sentence on p. 1525, line 15, right-hand column should read:

The flow in all of the cases studied is downward at the center of the fluid layer.